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METAL ION EXTRACTION BY SILYL-SUBSTITUTED DIPHOSPHONIC ACIDS. I. P,P'-DI-[3-(TRIMETHYLSILYL)-1-PROPYLENE] METHYLENE- AND ETHYLENEDIPHOSPHONIC ACIDS

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**METAL ION EXTRACTION BY
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ACIDS. I. P,P'-DI-
[3-(TRIMETHYLSILYL)-1-PROPYLENE]
METHYLENE- AND
ETHYLENEDIPHOSPHONIC ACIDS**

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ABSTRACT

In conjunction with efforts to develop novel actinide extractants that exhibit solubility in supercritical carbon dioxide (SCCO₂), the effect of adding silicon-based functionalities to diphosphonic acids on their aggregation and solvent extraction chemistry was investigated. Two silyl-derivatized diphosphonic acids, P,P'-di[3-(trimethylsilyl)-1-propylene] methylenediphosphonic acid (H₂DTMSP[MDP]) and P,P'-di[3-(trimethylsilyl)-1-propylene] ethylenediphosphonic acid (H₂DTMSP[EDP]), were prepared and their aggregation and metal ion extraction properties compared to those of the previously studied P,P'-di(2-ethylhexyl) alkylenediphos-

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phonic acids. Vapor pressure osmometry of H₂DTMSP[MDP] and H₂DTMSP[EDP] in toluene (25°C) indicates that, as is the case for the 2-ethylhexyl-substituted alkylendiphosphonic acid analogs, the compounds are dimeric and (primarily) hexameric, respectively, in the concentration range investigated. Distribution ratio measurements for the alkaline earth cations Ca²⁺, Sr²⁺, Ba²⁺, and Ra²⁺ as well as the representative tri-, tetra-, and hexavalent actinides Am³⁺, Th⁴⁺, and UO₂²⁺ between solutions of H₂DTMSP[MDP] and H₂DTMSP[EDP] in *o*-xylene and nitric acid indicate that the behavior of these silyl-derivatized compounds closely mimics that of the analogous P,P'-di(2-ethylhexyl) alkylendiphosphonic acids, indicating that incorporation of a silyl functionality has no adverse impact on the metal ion extraction properties of diphosphonic acids.

Key Words: Diphosphonic acids; Silyl-substituted; Metal ion extraction

INTRODUCTION

Over the last decade, diphosphonic acids have attracted considerable interest as metal ion complexing agents (1–5). Previous work in our laboratory has demonstrated that these compounds form remarkably stable complexes in acidic media with a variety of metal ions (e.g., actinides, lanthanides, and Fe(III)), a result of the strong acidity of the diphosphonic acid functionality and its ability to chelate metal ions through either its phosphoryl or ionized phosphonic acid groups (5,6). Although originally developed for use as aqueous complexing (i.e., “hold-back” or stripping) agents (2,7), diphosphonic acid ligands have subsequently been shown to provide the basis of several novel chelating ion-exchange resins (8–14), and upon appropriate alkyl substitution, they act as powerful metal ion extractants applicable in both extraction chromatography (15) and conventional liquid-liquid extraction (6,15–17).

During the past several years, supercritical carbon dioxide (SCCO₂) has received increasing attention as an environmentally friendly alternative to conventional organic solvents (18) in extraction processes. Unlike many solvents, SCCO₂ does not decompose into ozone-depleting fragments or promote the generation of photochemical smog. In addition, the use of SCCO₂ can lead to reduced waste stream volumes; if the applied pressure is lowered sufficiently, the carbon dioxide will revert to the gaseous state, allowing dissolved solutes to be collected as a liquid or solid residue and the CO₂ to be collected, repressurized, and reused. Carbon dioxide offers a number of other significant advantages as a solvent, among



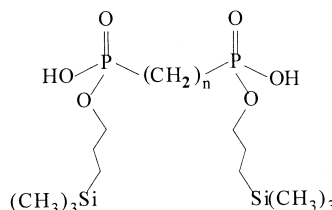
DIPHOSPHONIC ACID EXTRACTION. I

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them low cost, ready availability, comparatively low toxicity, favorable physical properties ($T_{\text{crit}} = 31.3^{\circ}\text{C}$; $P_{\text{crit}} = 72.9 \text{ atm}$), and in its supercritical state, relative ease of handling (using standard high-pressure equipment), low viscosity, and high diffusivity (18). Unfortunately, neither unsubstituted diphosphonic acids nor the alkyl-substituted acids reported to date (e.g., P,P'-di(2-ethylhexyl) alkylene-diphosphonic acids (6)) are soluble in unmodified SCCO_2 (19) because of its low solvent power. Although the solvent power of SCCO_2 can be improved by addition of an organic modifier (e.g., methanol), this approach is not always effective. Moreover, mixtures of conventional solvents with SCCO_2 are clearly less environmentally benign than SCCO_2 alone. For this reason, much effort has been directed at the development of metal ion complexing agents/extractants that incorporate CO_2 -philic substituents, which typically contain fluorine atoms or silicone polymer-based functionalities (20–31).

Recent work in our laboratory has focused on the preparation of diphosphonic acids that incorporate various silicon-based substituents (32) for possible application in SCCO_2 extraction. Such compounds are expected to be considerably less expensive than the analogous fluorinated diphosphonic acids, increasing the likelihood of eventual large-scale application. Moreover, while significant effort has been devoted to examination of the fluorination effect on metal ion complexation/extraction behavior and the SCCO_2 solubility of various ligands, relatively little work has been reported on the effect of adding silicon-based functional groups to the ligands. Until recently (32), no report had been made of an extant stable dialkyl alkylene-diphosphonic acid that contained a silicon moiety.

As a first step in evaluating the potential utility of silicon-derivatized diphosphonic acids as metal ion extractants in SCCO_2 , we have prepared 2 compounds containing the 3-(trimethylsilyl)-1-propyl group (Structure I, with $n = 1$ for $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $n = 2$ for $\text{H}_2\text{DTMSP}[\text{EDP}]$). Although our preliminary results indicated that the extractants are not appreciably soluble in SCCO_2 , we evaluated their metal ion extraction and aggregation properties in toluene-*o*-xylene. In this way, the behavior of these compounds can readily be compared to that of conventional dialkyl alkylene-diphosphonic acids (for which such data have been previously reported (6,16)) and the effect of the introduction of a silicon-



Structure I.



based functional group could be determined. The 3-(trimethylsilyl)-1-propyl group was selected for this work because the corresponding alcohol is commercially available and can be used to esterify diphosphonic acids through the use of well-established methodology (32). In addition, separating the trimethylsilyl functionality from the remainder of the molecule by 3 carbon atoms provides optimal chemical stability and synthetic accessibility (33).

EXPERIMENTAL

Materials

H₂DTMSP[MDP] and H₂DTMSP[EDP] were synthesized and characterized as described previously (32). The ligands were shown by potentiometric titration in methanol with standard base (J.T. Baker Chemical Co, Phillipsburg, NJ) to be greater than 97% pure. Sucrose octaacetate (Jupiter Instrument Co) and solutions prepared from Baker-analyzed PHOTREX grade toluene (Aldrich Chemical Co, Milwaukee, Wis) were used without further purification for the vapor pressure osmometry (VPO) measurements. Aqueous solutions were prepared with water from a Milli-Q2 purification system and Ultrex reagent nitric acid (J. T. Baker Chemical Co). The organic solutions used in solvent extraction experiments were prepared by dissolving a known mass of the extractant in sufficient *o*-xylene (Aldrich) to achieve the desired molarity. ⁴⁵Ca, ⁸⁵Sr, and ¹³³Ba were obtained from Isotope Products Laboratories (Burbank, Calif). ²²³Ra was separated from ²²⁷Ac through the use of an extraction chromatographic column that contained bis(2-ethylhexyl) phosphoric acid. The radioisotopes ²⁴¹Am, ²³³U, and ²³⁰Th were obtained from Argonne National Laboratory stocks. Only freshly purified ²³³U and ²³⁰Th were used in the extraction experiments. The radioisotopes were used at tracer level concentration, with the exception of ²³³U and ²³⁰Th, which were used in the solvent extraction experiments at a concentration of 10⁻⁵ to 10⁻⁴ mol/L.

Methods

The aggregation of H₂DTMSP[MDP] and H₂DTMSP[EDP] in toluene at 25°C was measured by VPO with a Jupiter Model 833 vapor pressure osmometer as described previously (34). The instrument was calibrated with standard toluene solutions of sucrose octaacetate. A plot of measured voltage versus sucrose octaacetate molality (m) gave a slope of 1788 μV/m for the instrument calibration constant.

The metal distribution ratios were measured as described for the di(2-ethylhexyl) alkylendiphosphonic acids (6,16,17). The distribution ratio, *D*, was calculated as the ratio of the activity of a radiotracer between an *o*-xylene solution of



the extractant and an aqueous nitric acid solution. Preliminary experiments showed that 5 minutes of vortexing was more than enough time to attain equilibrium. Duplicate experiments showed that the reproducibility of the D measurements was generally within 5%; however, the uncertainty interval was higher for the highest D values ($D > 10^3$).

RESULTS AND DISCUSSION

Aggregation

Figure 1 shows a comparison of the results of the VPO measurements for $H_2DTMSP[MDP]$ and $H_2DTMSP[EDP]$ with those for the monomeric standard sucrose octaacetate. As in the case of the analogous P,P' -di(2-ethylhexyl) methylenediphosphonic acid ($H_2DEH[MDP]$) (34), the VPO data indicate that $H_2DTMSP[MDP]$ is dimeric in toluene at 25°C in the 0.01–0.12 m concentration range. The linearity of the data indicates that the aggregation constant is sufficiently large such that the extractant aggregation remains unchanged over the concentration range studied.

The VPO data for $H_2DTMSP[EDP]$, in contrast to those observed for $H_2DTMSP[MDP]$, are not linear. The best straight-line fit of the data has a slope

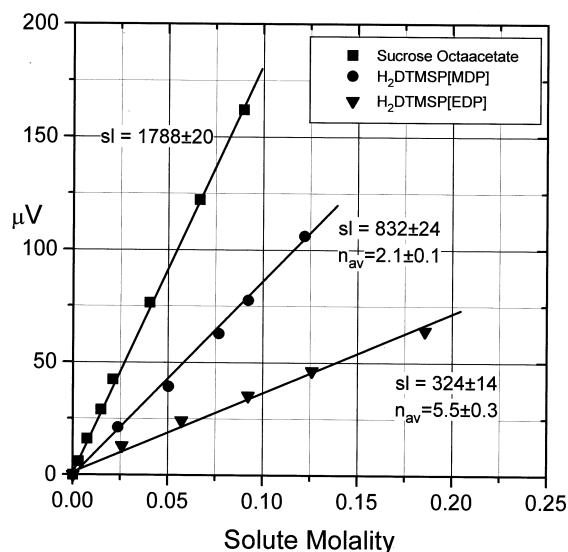


Figure 1. VPO measurements (microvolts, μV , vs. molality, m) with $H_2DTMSP[MDP]$, $H_2DTMSP[EDP]$, and the monomeric standard sucrose octaacetate in toluene at 25°C .



consistent with an average aggregation number (n_{av}) of approximately 5.5. This strongly suggests the formation of hexameric aggregates analogous to those observed for P,P'-di(2-ethylhexyl) ethylenediphosphonic acid (H₂DEH[EDP]) (34). For a more quantitative description of the aggregation equilibrium of H₂DTMSP[EDP] in toluene at 25°C, the VPO data are reported in Fig. 2a as the average degree of aggregation (n_{av}) versus the solute molality. The average degree of aggregation is defined as

$$n_{av} = \frac{C_{tot}}{S} = \frac{C_{tot}}{\left(\frac{\mu V}{K_r}\right)} \quad (1)$$

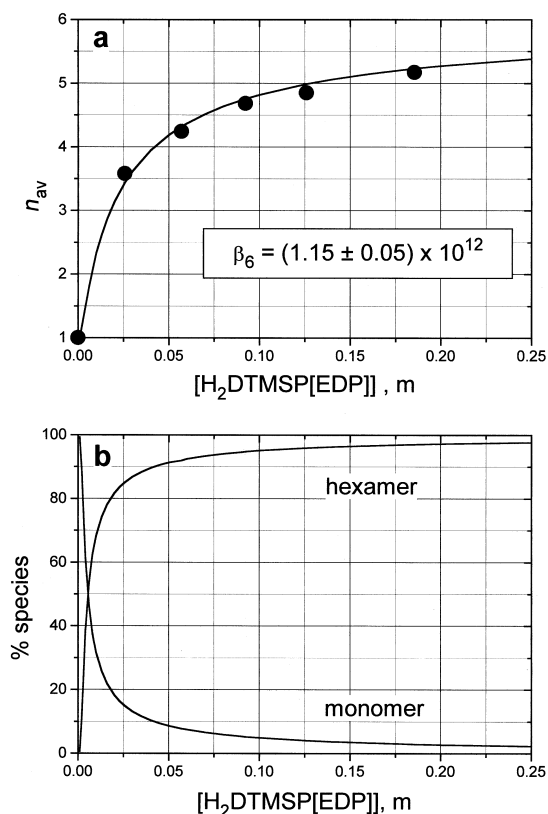


Figure 2. a) Best fit of aggregation data, average aggregation number (n_{av}) vs. molality (m), for H₂DTMSP[EDP]; b) Distribution of H₂DTMSP[EDP] between monomeric and hexameric species as a function of total solute concentration.



where C_{tot} is the known analytical concentration of $\text{H}_2\text{DTMSP}[\text{EDP}]$, and S is the sum of the concentration of each species present in the system. For each data point in Fig. 1, an experimental value of S is obtained by dividing the instrument reading (μV) by the slope of the sucrose octaacetate reference line ($K_r = 1788$).

C_{tot} and S can be expressed through the following mass balance equations and equilibrium aggregation constants (β_n) :

$$C_{\text{tot}} = a + n \sum \beta_n a^n \quad (2)$$

$$S = a + \sum \beta_n a^n \quad (3)$$

where a represents the monomer concentration.

To calculate the β_n values that best describe the experimental values of Fig. 2a, the procedure and calculations described in (17) were used. Several aggregation models involving dimers, trimers, tetramers, and hexamers were tested. The results of the calculations indicate that the model that best describes the aggregation of $\text{H}_2\text{DTMSP}[\text{EDP}]$ in toluene involves only the formation of a hexameric species with $\beta_6 = 1.15 (\pm 0.05) \times 10^{12}$. A comparison of the experimental data with the calculated curve is shown in Fig. 2a.

The value of β_6 for $\text{H}_2\text{DTMSP}[\text{EDP}]$ is more than one order of magnitude lower than that reported previously for $\text{H}_2\text{DEH}[\text{EDP}]$ ($6(\pm 1) \times 10^{13}$ (16)). $\text{H}_2\text{DTMSP}[\text{EDP}]$ thus has a somewhat lower tendency to aggregate than its 2-ethylhexyl analogue. Fig. 2b shows the species distribution diagram for $\text{H}_2\text{TMSP}[\text{EDP}]$ in toluene calculated with the β_6 value reported above. It appears from the figure that, although the hexamer is the predominant species under most conditions, at very low extractant concentrations the presence of monomeric $\text{H}_2\text{DTMSP}[\text{EDP}]$ is not negligible and must be taken into account to explain some features of the extraction data.

Solvent Extraction Studies

Alkaline Earth Cations

Figures 3 and 4 show the acid dependency data at 0.1 mol/L extractant and the extractant dependency data at 0.05 mol/L HNO_3 for selected alkaline earth cations with $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$, respectively. These data indicate that these extractants behave very similarly to the analogous di(2-ethylhexyl) alkylendiphosphonic acid extractants (6,16). The acid dependencies for both extractants exhibit a slope of -2 , which is consistent with the displacement of 2 protons by a divalent metal cation upon extraction into the organic phase.

The extractant dependencies for $\text{H}_2\text{DTMSP}[\text{MDP}]$ show a variable slope. This slope is close to 2 in the 0.001–0.01 M concentration range and is slightly lower at higher extractant concentrations. This phenomenon was also observed



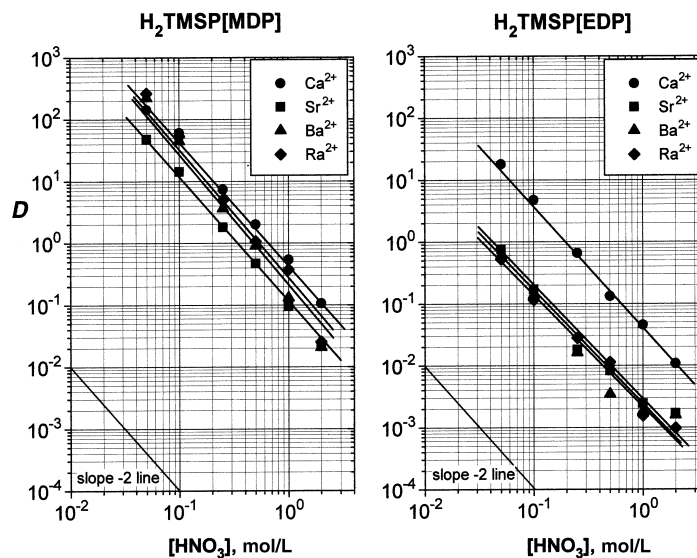


Figure 3. Acid dependencies at 25°C for the extraction of selected alkaline earth cations by 0.1 mol/L $\text{H}_2\text{DTMSP[MDP]}$ and $\text{H}_2\text{DTMSP[EDP]}$ in *o*-xylene.

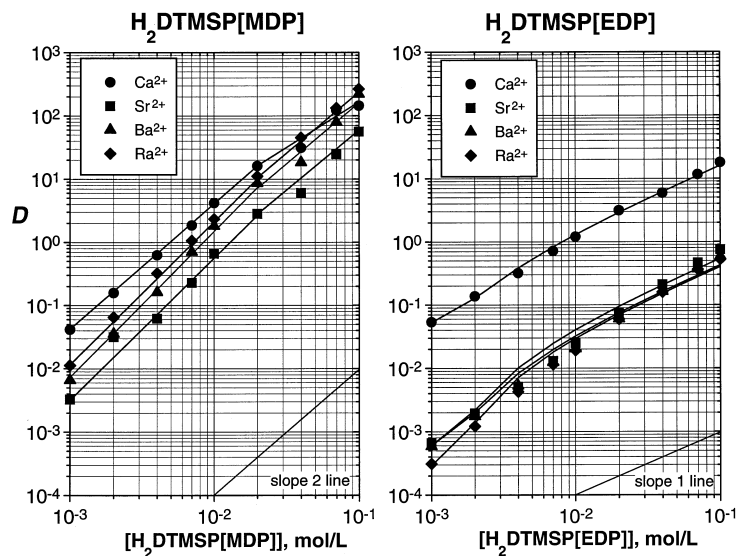


Figure 4. Extractant dependencies at 25°C for the extraction of selected alkaline earth cations by $\text{H}_2\text{DTMSP[MDP]}$ and $\text{H}_2\text{DTMSP[EDP]}$ in *o*-xylene from 0.05 mol/L HNO_3 .



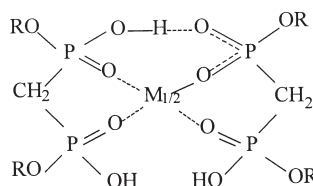
with H₂DEH[MDP] and was attributed to significant solubility of metal-ligand complexes in the aqueous phase (6). However, in the case of H₂DTMSP[MDP], the observed variation in the slope of the extractant dependency at higher extractant concentrations is smaller than that observed for H₂DEH[MDP]. This implies that the alkaline earth—H₂DTMSP[MDP] complexes are less soluble in the aqueous phase than are the analogous H₂DEH[MDP] complexes, a phenomenon which was also noted in qualitative solubility tests during the synthesis of H₂DTMSP[MDP] (35) and H₂DEH[MDP] (36) salts for study by infrared spectroscopy. The lower solubility of the silyl-substituted alkaline earth diphosphonic acid complexes in the aqueous phase may also explain why the extraction of alkaline earth cations by H₂DTMSP[MDP] or H₂DTMSP[EDP] yields *D* values that are typically 2 to 3 times higher than in alkaline earth extraction with H₂DEH[MDP] or H₂DEH[EDP], respectively, under identical conditions.

Because H₂DTMSP[MDP] has been shown by VPO to be dimeric in the concentration range over which the extractant dependencies were determined, the slope of approximately 2 for the extractant dependency indicates that each divalent alkaline earth cation is extracted by 2 H₂DTMSP[MDP] dimers. Therefore, as in the case of H₂DEH[MDP] (6), the stoichiometry of alkaline-earth cation extraction with H₂DTMSP[MDP] can be expressed as



where overbars indicate organic phase species and H₂Y represents H₂DTMSP[MDP]. Structure II was proposed (6) for the extraction of alkaline earth cations by H₂DEH[MDP] and is very likely applicable for H₂DTMSP[MDP] as well. (For clarity, only one of the mono-deprotonated dimer units has been shown.) In this structure, 2 protons are displaced from 2 dimers of the extractant, as required by the slope analysis (i.e., -2 and 2 for the measured acid and extractant dependencies, respectively). The 6-member chelate rings shown in Structure II arise from the interaction of the metal ion with the phosphoryl oxygens of the extractant.

The extractant dependencies for H₂DTMSP[EDP] have a limiting slope of 1 in the 0.01–0.1 mol/L concentration range. As in the extraction of alkaline earth metals with H₂DEH[EDP], the slope increases at low extractant concentrations. A slope of 1 in the log-log plot of metal distribution ratio versus the analytical con-



Structure II.



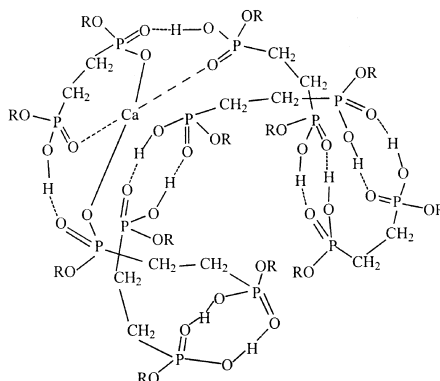
centration of the extractant is consistent with extraction by a highly aggregated species in which the aggregation is not disrupted by the metal ion (16). This result is in agreement with the VPO data, which indicate that $\text{H}_2\text{DTMSP}[\text{EDP}]$ is primarily hexameric over the concentration range studied (Fig. 2b).

The extraction of alkaline earth cations by the $\text{H}_2\text{DTMSP}[\text{EDP}]$ hexamer can therefore be expressed as



where $(\text{H}_2\text{Y})_6$ is the hexameric $\text{H}_2\text{DTMSP}[\text{EDP}]$ aggregate and $\overline{\text{MH}_{10}\text{Y}_6}$ is the metal-hexamer complex in the organic phase. As required by the slope of -2 in the acid dependency plot, 2 protons are lost by the hexamer upon complexation of an alkaline earth cation. Infrared spectroscopy (34) and small angle neutron scattering (37,38) experiments with $\text{H}_2\text{DEH}[\text{EDP}]$ in toluene suggest a spherical morphology for the hexamer and the extracted alkaline-earth metal complexes (Structure III). In this structure, an alkaline earth metal cation lies in a hydrophilic cavity formed by the $\text{H}_2\text{DTMSP}[\text{EDP}]$ aggregate, which resembles a reverse micelle. A number of 7- and 8-membered chelate rings are formed in this structure through coordination to the diphosphonate ligand. The remaining coordination sites on the metal ion may be occupied by water molecules, which are not shown for clarity. Although these experiments could not be repeated for $\text{H}_2\text{DTMSP}[\text{EDP}]$ because of the low solubility of the metal complexes, we have made the reasonable assumption that the $\text{H}_2\text{DTMSP}[\text{EDP}]$ aggregate adopts a similar structure.

The higher slope values in the 0.001–0.005 mol/L concentration range of the $\text{H}_2\text{DTMSP}[\text{EDP}]$ —alkaline-earth extractant dependencies can be attributed to incomplete aggregation of the extractant. In this region, where the concentration of monomeric extractant is not negligible (Fig. 2b), the measured D values include contributions of both equilibrium (Eq. 5) and extraction by the monomeric ex-



Structure III.

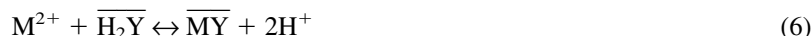


Table 1. Equilibrium Constants for the Extraction of Alkaline Earth Cations by the Monomeric and Hexameric Forms of H₂DTMSP[EDP]

Cation	$K_{\text{ex,mon}}$	$K_{\text{ex,hex}}$
Ca	$(1.3 \pm 0.3) \times 10^{-1}$	$(2.49 \pm 0.05) \times 10$
Sr	$(1.4 \pm 1.4) \times 10^{-3}$	$(8.5 \pm 1.0) \times 10^{-2}$
Ba	$(1.4 \pm 1.4) \times 10^{-3}$	$(6.7 \pm 1.0) \times 10^{-2}$
Ra	$(7 \pm 7) \times 10^{-4}$	$(6.3 \pm 1.0) \times 10^{-2}$

Constants calculated from data of Fig. 4 and (Eqs. 5 and 6).

tractant. The reaction can be written as



Studies of metal ion extraction using *n*-decanol (39), a diluent in which the extractants are monomeric (40), verify that alkaline earth cations are readily extracted by monomeric diphosphonic acids.

The nonlinear least-squares curve-fitting feature of Origin® (Version 3.5, Microcal Software Inc, Northampton, Mass) was used to analyze the extractant dependency data for H₂DTMSP[EDP] given in Fig. 4. The best fit of the data was obtained using equilibria (Eqs. 5 and 6) and the β_6 value determined from the VPO data (Fig. 2a). We performed the calculations while under the assumption that the extent of extractant aggregation in toluene and *o*-xylene is the same and that all species behave ideally. The equilibrium constants provided by these calculations are reported in Table 1. The curves pictured in the H₂DTMSP[EDP] extractant dependency plot (Fig. 4) have been calculated using these equilibrium constants. The very high standard deviations obtained for $K_{\text{ex, mon}}$ stem from the few experimental points that are available in the extractant concentration range where reaction (Eq. 6) contributes significantly to the measured *D* values. Other stoichiometries for equilibrium (Eq. 6), such as that involving the extraction of the cation by 2 monomers of H₂DTMSP[EDP], provided a less satisfactory fit of the data.

As with the analogous di(2-ethylhexyl)-substituted extractants (6,16), the introduction of an additional CH₂ group into the alkylene bridge separating the phosphoryl groups profoundly affects alkaline earth extraction. H₂DTMSP[MDP] and H₂DEH[MDP] exhibit virtually no selectivity over the series of alkaline earths, while H₂DTMSP[EDP] and H₂DEH[EDP] behave in a manner similar to monofunctional extractants (41,42) and preferentially extract Ca. This behavior seems to indicate that the ethylenediphosphonic acids exhibit at least some monofunctional character.

Extraction of Ca with H₂DTMSP[EDP] yields *D* values typically 30 times higher than for Sr, Ba, or Ra. However, this selectivity is accompanied by lower *D* values than does extraction with H₂DTMSP[MDP]. Extraction with



$\text{H}_2\text{DTMSP}[\text{MDP}]$ yields D values that are 10 times higher for Ca and 100 times higher for Sr, Ba, and Ra than those obtained in extraction with $\text{H}_2\text{DTMSP}[\text{EDP}]$ under the same conditions. If one considers the proposed Structures II and III, the lower D values exhibited by $\text{H}_2\text{DTMSP}[\text{EDP}]$ would be expected due to the formation of 7-member chelate rings rather than the more stable 6-member chelate rings formed by $\text{H}_2\text{DTMSP}[\text{MDP}]$ (16).

Actinides

Figure 5 shows the nitric acid dependencies for the extraction of representative tri-, tetra-, and hexavalent actinides by 0.01 mol/L $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$ solutions in *o*-xylene. These data are very similar to those observed for the di(2-ethylhexyl)-substituted diphosphonic acid extractants (6,16).

The acid dependency data for the extraction of Am(III) by $\text{H}_2\text{DTMSP}[\text{MDP}]$ exhibit a maximum at 0.2–0.3 mol/L HNO_3 . This feature of the data, which differs from the expected acid dependency for a trivalent metal cation (i.e., a straight line with a slope of -3), was also observed with the $\text{H}_2\text{DEH}[\text{MDP}]$ -Am(III) system and could arise for several reasons. For example, species of different stoichiometries may be formed at different acid concentrations. In the 0.05–0.3 mol/L HNO_3 concentration range, a positively charged complex (e.g., 1:1 ligand-metal) could form

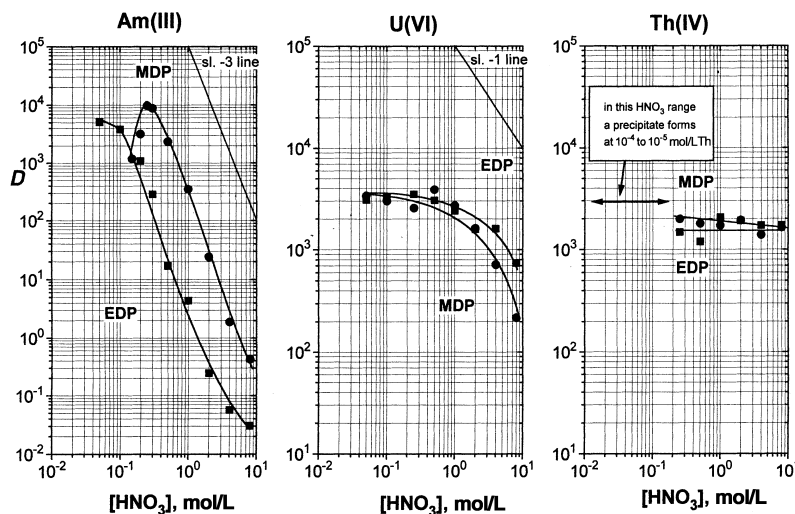


Figure 5. Acid dependencies at 25°C for the extraction of Am(III), U(VI), and Th(IV) by 0.01 mol/L $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$ in *o*-xylene.



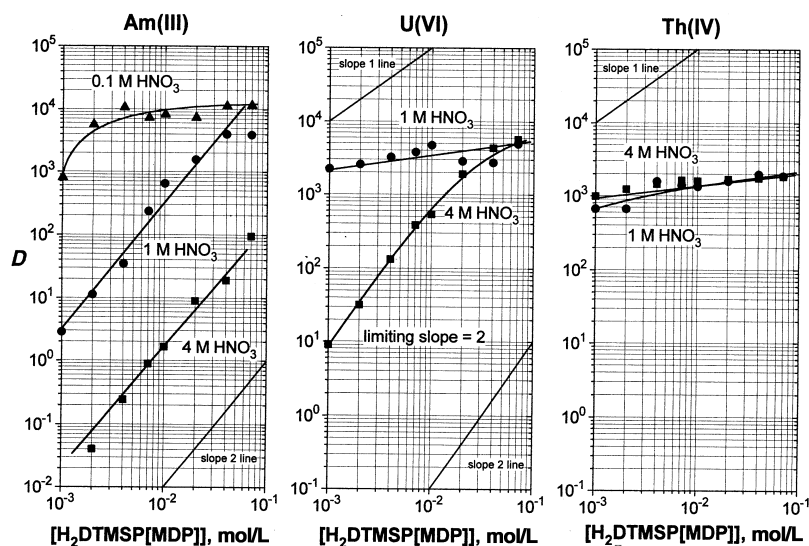


Figure 6. Extractant dependencies for the extraction of Am(III), U(VI), and Th(IV) by $\text{H}_2\text{DTMSP[MDP]}$ in *o*-xylene from various concentrations ($M = \text{mol/L}$) of HNO_3 .

and preferentially report to the aqueous phase. Extraction of this species into the organic phase would depend on the availability of the nitrate ion for charge neutralization. The value of the distribution ratio would therefore increase with nitric acid concentration. At higher acidities, a neutral complex (2:1 ligand-metal) that preferentially reports to the organic phase could be formed, leading to the expected acid dependency slope of -3 . Alternatively, the formation of complexes with different degrees of protonation could be involved. At the lowest acidities, the ligand likely exists as the completely deprotonated dianion (DTMSP[MDP]^{2-}), while at higher acidities, the predominant ligand species would be the monoprotonated anion (HDTMSP[MDP]^{1-}). Because $\text{p}K_a$ values for these diphosphonic acids are not available, we could not derive quantitative speciation information from the distribution data.

The possible formation of complexes with different ligand-to-metal stoichiometries is qualitatively supported by the extractant dependency data for $\text{H}_2\text{DTMSP[MDP]}$ and Am(III) shown in Fig. 6. Extractant dependencies at 1 and 4 mol/L HNO_3 , the acid concentration region in which the observed slope for the acid dependency plot is -3 , exhibit slopes of 2. This indicates complexation by 2 $\text{H}_2\text{DTMSP[MDP]}$ dimers from which 3 protons have been displaced to form complexes similar to Structure II. At 0.1 mol/L HNO_3 , the extractant dependency data exhibit a slope of approximately 1 at low extractant concentrations, suggest-



ing the formation of complexes of lower stoichiometry (i.e., a 1:1 ligand-metal complex). At higher extractant concentrations, the Am(III)-H₂DTMSP[MDP] distribution values at 0.1 mol/L HNO₃ are nearly constant, an observation consistent with significant aqueous phase solubility of the 1:1 ligand-metal complex. However, *D* values higher than 10⁴ are subject to considerable uncertainty because the metal ion concentration in the aqueous phase is close to the detection limit normally achievable using reasonable amounts of radioactive tracers.

The acid dependency data observed for Am(III) extraction by H₂DTMSP[EDP] are closer to those expected for a trivalent cation (i.e., an observed slope of -3 over nearly the entire acid concentration range). At low acidities, the *D* values for the extraction of Am(III) by H₂DTMSP[EDP] (Fig. 5) exceed those for H₂DTMSP[MDP], while at high acidities *D* values are approximately 100 times lower for H₂DTMSP[EDP] than they are for H₂DTMSP[MDP]. As was the case for alkaline earth cations (see above), this behavior can be rationalized on the basis of 7-member chelate ring formation by H₂DTMSP[EDP] (Structure III), rather than the 6-member chelate rings possible with H₂DTMSP[MDP] (16).

The extractant dependency data for Am(III) at 1 and 4 mol/L HNO₃ with H₂DTMSP[EDP], shown in Fig. 7, exhibit slopes of 1 in the 0.01–0.1 mol/L concentration range. As observed for alkaline-earth cation extraction with this compound, at lower extractant concentrations (0.001–0.01 mol/L), the extractant de-

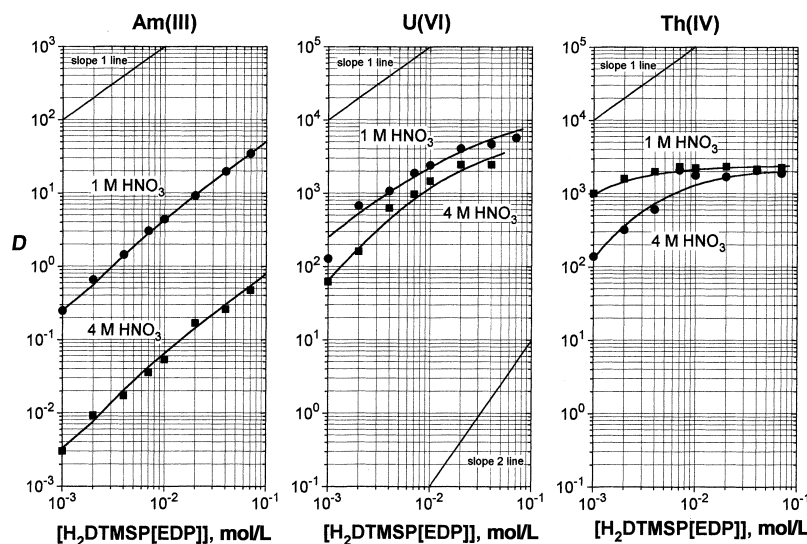


Figure 7. Extractant dependencies at 25°C for the extraction of Am(III), U(VI), and Th(IV) by H₂DTMSP[EDP] in *o*-xylene from 1 and 4 mol/L HNO₃.

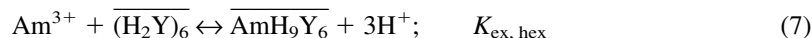


Table 2. Equilibrium Constants for the Extraction of Am(III) by the Monomeric and Hexameric Forms of H₂DTMSP[EDP]

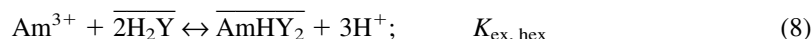
[HNO ₃], mol/L	K _{ex,mon}	K _{ex,hex}
1	$(1.8 \pm 0.3) \times 10^5$	$(2.55 \pm 0.05) \times 10^3$
4	$(1.4 \pm 0.5) \times 10^5$	$(2.16 \pm 0.08) \times 10^3$

Constants calculated from data of Fig. 7 and (Eqs. 7 and 8).

pendency data exhibit greater slopes due to incomplete ligand aggregation. In this region, both the monomeric and the hexameric species contribute to metal extraction according to the equilibrium equations



and



Through the procedure described above for the alkaline-earth cation extraction by H₂DTMSP[EDP], the β_6 value of H₂DTMSP[EDP] and equilibria (Eqs. 7 and 8) were used to fit the Am(III) extractant dependency data of Fig. 7. The values obtained for the equilibrium constants for Eqs. (7 and 8) are reported in Table 2. The curves shown in Fig. 7 for the Am(III) extractant dependencies were calculated using these values.

The data for U(VI) and Th(IV) extraction with H₂DTMSP[MDP] and H₂DTMSP[EDP] shown in Figs. 5–7 are very similar to those obtained with the analogous di(2-ethylhexyl) alkylendiphosphonic acids (6,16). Overall, the extraction data suggest that these metal complexes have a pronounced tendency to polymerize and exist in solution as a mixture of complexes with various stoichiometries and degrees of ligand protonation. The limited (U(VI)) or complete lack (Th(IV)) of acid dependency shown in Fig. 5 suggest that extraction of these metal ions by H₂DTMSP[MDP] and H₂DTMSP[EDP] occurs primarily through the phosphoryl oxygens of the fully protonated extractant. The U(VI) data show some acid dependency at higher acidities, where the slope approaches unity, suggesting partial deprotonation of the extractant and/or competition for the phosphoryl group from HNO₃.

The extractant dependency data for U(VI) exhibit variable slopes. At 4 mol/L HNO₃, the dependencies for H₂DTMSP[MDP] and H₂DTMSP[EDP] exhibit limiting slopes of 2 and 1, respectively. At 1 mol/L HNO₃, the slope decreases slightly for H₂DTMSP[EDP], while the H₂DTMSP[MDP] data become almost independent of the extractant concentration. Slope values close to unity are expected for the U(VI)-H₂DTMSP[EDP] extractant dependency data because the extractant is highly aggregated (16). Although the U(VI) data exhibit a limiting



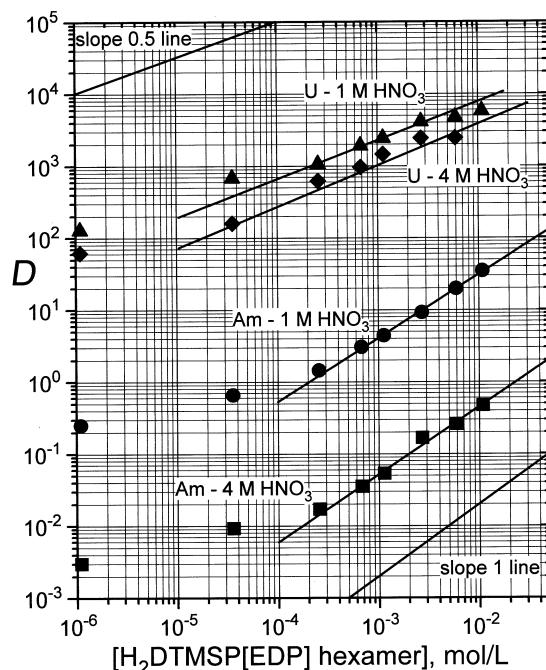
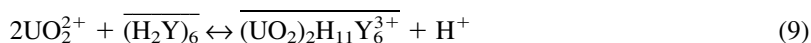


Figure 8. Distribution ratio, D , vs. hexamer concentration for the extraction of Am(III) and U(VI) at 25°C by $H_2DTMSP[EDP]$ in o -xylene from 1 and 4 mol/L HNO_3 .

slope of unity at low $H_2DTMSP[EDP]$ concentration, the slope decreases at higher extractant concentrations.

To gain further insight into the U(VI)- $H_2DTMSP[EDP]$ system, the extractant dependency data of Fig. 7 were plotted in Fig. 8 as a function of the $H_2DTMSP[EDP]$ hexamer concentration. At each analytical concentration of the extractant, the hexamer concentration was calculated with the β_6 value of $H_2DTMSP[EDP]$. The Am(III) data are also shown in Fig. 8 to contrast the behavior of these 2 actinide ions. The Am(III) data are linear with a slope of unity, except at very low extractant concentrations, where extraction by monomeric $H_2DTMSP[EDP]$ contributes significantly to the measured D values. The U(VI) data are also linear, but exhibit slopes of only 0.5. This slope is consistent with Eq. (9):



and implies that 2 uranyl ions are extracted by each hexameric aggregate. As depicted in this equation, a single proton is displaced from the hexamer, which is



consistent with the slope one observed from 1 to 4 mol/L HNO_3 in the $\text{H}_2\text{DTMSP}[\text{EDP}]$ acid dependency plots. The remaining charge on the uranyl complex would be neutralized by nitrate anions. The lines fitting the U(VI) data of Fig. 8 were calculated based on equilibrium (Eq. 9) with values for the equilibrium constant equal to $4.0 (\pm 0.5) \times 10^4$ at 1 mol/L HNO_3 and $6.0 (\pm 1.0) \times 10^4$ at 4 mol/L HNO_3 , respectively. In Fig. 8, the positive deviation of the U(VI) data from the calculated lines at the lowest extractant concentrations may be attributed to metal extraction by the monomeric extractant. However, the deviation from linearity is less pronounced than it is for Am(III) , undoubtedly due to the much higher affinity of the monomeric extractant for U(VI) .

The extraction of Th(IV) by $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$ is independent of extractant concentration. This behavior is indicative of the formation of a new phase (a colloidal phase or a precipitate) in the extraction system. Under these conditions, the system becomes zero-variant. During collection of the acid dependency data of Fig. 5, this new phase manifested itself, at aqueous acidities below 0.2 mol/L, as cloudiness in the aqueous phase. This cloudiness most likely arises from precipitation of a Th(IV) -diphosphonate complex. Similar observations were noted with the di(2-ethylhexyl) analogues (6,16). The tendency of Th(IV) to form large polymeric aggregates with $\text{H}_2\text{DEH}[\text{MDP}]$ in the organic phase was previously established through small-angle neutron scattering measurements (38), and $\text{H}_2\text{DTMSP}[\text{MDP}]$ appears to exhibit the same behavior.

CONCLUSIONS

The aggregation and solvent extraction properties of 2 novel silicon-substituted diphosphonic acids, $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$, were found to closely mimic those of analogous di(2-ethylhexyl) alkylendiphosphonic acids. As observed for di(2-ethylhexyl)-substituted extractants, the introduction of an additional CH_2 group into the alkylene bridge separating the phosphoryl groups profoundly affects the aggregation and solvent extraction properties of these silyl-substituted alkylendiphosphonic acids. VPO studies in toluene at 25°C indicate that $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$ are dimeric and (primarily) hexameric, respectively, over the concentration range studied. Nonlinear least-squares fitting of the VPO data for $\text{H}_2\text{DTMSP}[\text{EDP}]$ yielded an estimated aggregation equilibrium constant (β_6) of $1.15 (\pm 0.05) \times 10^{12}$.

Extraction of alkaline earth cations from nitric acid into *o*-xylene solutions of the 2 extractants yields acid dependencies exhibiting slopes of -2 for both compounds and extractant dependencies of slope 2 and 1 for $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$, respectively. These results suggest that the extraction of alkaline earth cations by $\text{H}_2\text{DTMSP}[\text{MDP}]$ involves 2 mono-deprotonated dimers, while extraction by $\text{H}_2\text{DTMSP}[\text{EDP}]$ involves a doubly deprotonated hexamer.



While $\text{H}_2\text{DTMSP}[\text{MDP}]$ exhibits no selectivity over the series of alkaline earth cations studied, $\text{H}_2\text{DTMSP}[\text{EDP}]$ preferentially extracts Ca over Sr, Ba, and Ra, much like a monofunctional organophosphorus extractant. The lower distribution ratios observed for alkaline earth extraction by $\text{H}_2\text{DTMSP}[\text{EDP}]$ can be attributed to the formation of 7-member chelate rings, which are expected to be much less stable than the 6-member chelate rings possible with $\text{H}_2\text{DTMSP}[\text{MDP}]$.

Extraction of Am(III) with $\text{H}_2\text{DTMSP}[\text{MDP}]$ yields an acid dependency with a maximum at 0.2–0.3 mol/L HNO_3 and extractant dependencies in which slopes vary with acidity. This unusual behavior was attributed to the formation of positively charged species at low acidity that report preferentially to the aqueous phase. Extraction of Am(III) with $\text{H}_2\text{DTMSP}[\text{EDP}]$ yields an acid dependency with a slope of -3 and an extractant dependency of unit slope, indicating complexation by a hexameric aggregate of $\text{H}_2\text{DTMSP}[\text{EDP}]$ from which 3 protons have been displaced.

U(VI) and Th(IV) extraction with $\text{H}_2\text{DTMSP}[\text{MDP}]$ and $\text{H}_2\text{DTMSP}[\text{EDP}]$ exhibit little or no acid dependency, suggesting that metal complexation in these cases occurs predominantly through the interaction of the metal ion with the phosphoryl oxygens of the fully protonated extractant. The variable slopes exhibited by the U(VI) extractant dependency data suggest the formation of complexes of various stoichiometries and degrees of protonation, while the lack of extractant dependency exhibited by the extraction of Th(IV) indicates the formation of colloidal or solid species.

Taken together, these results clearly demonstrate that incorporation of a silicon-based functionality into a diphosphonic acid does not adversely affect its metal ion extraction behavior. Although our preliminary results indicate that the extractants considered here are not appreciably soluble in SCCO_2 (19), we expect that this can be remedied by use of an appropriate phase modifier or introduction of additional functional groups onto the diphosphonic acid backbone. Work addressing these opportunities is now underway in our laboratory.

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